

16-CHEM-A2, UNIT OPERATIONS and SEPARATION PROCESSES

DECEMBER 2017

3 hours duration

NOTES

1. If doubt exists as to the interpretation of any question, the candidate is urged to submit with the answer paper, a clear statement of any assumptions made.
2. The examination is an **open book exam**. One textbook of your choice with notations listed on the margins etc., but no loose notes are permitted into the exam.
3. Candidates may use any **non-communicating** scientific calculator.
4. All problems are worth 25 points. At least **two problems** from **each** of parts **A** and **B** must be attempted.
5. **Only the first two** questions as they appear in the answer book from each section will be marked.
6. State all assumptions clearly.

PART A: UNIT OPERATIONS

- A1.** Bench tests were done on a new valve to determine the energy loss as a function of valve closure. This involves mounting the valve into a plumbing system and measuring the flow rate through the valve and supplying a flow of water with a constant head of 1.5 m from an overhead tank. The valve is fitted to a 1.5-meter long, 20-mm internal diameter horizontal smooth-walled pipe. The following test data was obtained:

Valve Closure, in %	Water Flow Rate, in m ³ /min
0	8.4 x 10 ⁻²
25	6.0 x 10 ⁻²
40	3.6 x 10 ⁻²

Calculate the loss factor (k_v) for each valve closure position using the following equation for head loss (h):

$$h = k_v (u^2/2g)$$

where u is the average velocity of flowing water and g is the acceleration due to gravity.

DATA: Density of water = 1000 kg/m³
 Viscosity of water = 1 x 10⁻³ N.s/m²

- A2. A centrifugal pump operating at 2500 rpm was used to provide experimental data of flow as well as delivery pressure and torque on the rotating shaft. The performance of the pump is as follows:

Volumetric Flow Rate (in m^3/s)	Differential Pressure (in kN/m^2)	Force on Arm (in N)
1.47×10^{-3}	18.8	4.6
1.31×10^{-3}	36.0	4.1
1.18×10^{-3}	44.8	4.0
1.00×10^{-3}	61.5	3.7
0.91×10^{-3}	63.6	3.3
0.71×10^{-3}	71.5	3.0
0.48×10^{-3}	79.7	2.4

The force on a torque arm linked to the pump has a length of 17.9 cm as measured from the axis of the rotating shaft. Determine the maximum efficiency of the pump and the corresponding flow rate.

- A3. Continuous separation of spherical particles of waste ore in wash water is accomplished in a rectangular lagoon (10 m wide x 50 m long x 2 m deep). The ore particles are suspended in the flow of the wash water at a rate of $360 \text{ m}^3/\text{hr}$. Determine the size of the ore particle that can be retained by the lagoon if the maximum ore particle size obeys Stoke's law for a particle Reynolds number below a value of 0.4.

DATA: Viscosity of wash water = $1 \times 10^{-3} \text{ N.s/m}^2$
 Density of ore = 2.8 g/cc
 Density of wash water = 1.0 g/cc

PART B: SEPARATION PROCESSES

- B1.** 96% of acetone (C_3H_6O) is to be absorbed from a 2% by mole mixture of acetone in air in a continuous countercurrent absorption tower using 20% more than the minimum liquid rate of pure water as the solvent, which is introduced at the top of the tower. The gas mixture is blown into the bottom of the tower at a flow rate of 450 kg/hr. The absorption tower, which operates at atmospheric pressure and 300K, is packed with 2.54 cm Raschig rings. The equilibrium relation is $y = 2.5x$, where y and x are mole fractions of acetone in air and water, respectively. The following relationship is available for height of a transfer unit based on overall resistance in terms of gas/vapor phase (H_{oy}):

$$H_{oy} = H_y + \{(mG/L) H_x\}$$

where

$H_y \rightarrow$ height of a transfer unit based on resistance in terms of gas/vapor phase = 0.54 m

$H_x \rightarrow$ height of a transfer unit based on resistance in terms of liquid phase = 0.32 m

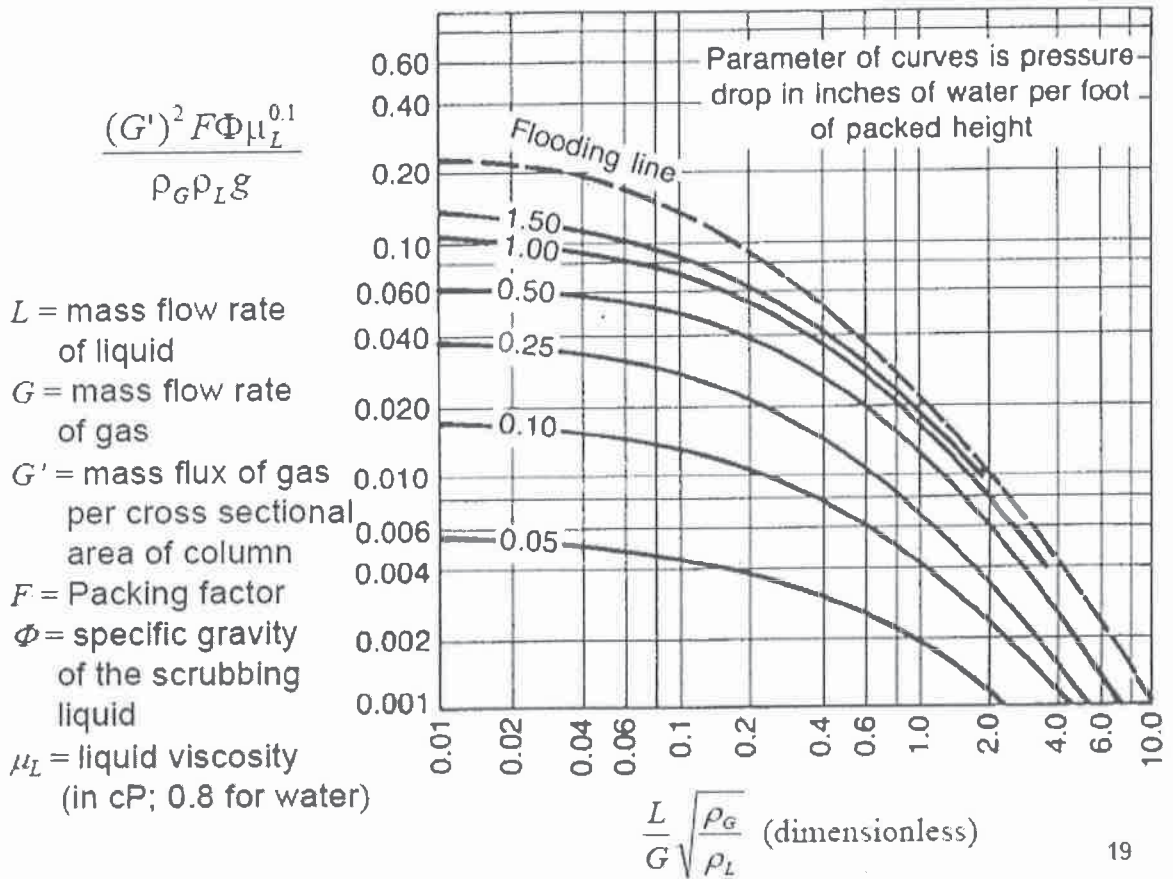
$m \rightarrow$ slope of equilibrium line

$G \rightarrow$ mass flow rate of gas/vapor phase

$L \rightarrow$ mass flow rate of liquid phase

- (a) [15 points] Find the height of absorption tower.
- (b) [10 points] Find the diameter of the absorption tower operating at 50% of the flooding velocity.

DATA: Viscosity of solution (μ_L) = 0.86 cP
 Density of acetone-air mixture (ρ_G) = 1.181 kg/m³
 Density of pure water and acetone-water solution (ρ_L) = 998.4 kg/m³
 Characteristic packing factor (F) = 160
 Specific gravity of water = 1.0



Sherwood Flooding Correlation for Packed Towers

"Packed Tower Design and Applications" By Ralph E. Stigle, Jr., Gulf Publishing Company, Houston, Texas, 1996.

- B2.** A wet slab of material (0.35 m^2 area and 7 mm thick) was batch dried, and the drying rate (N) in $\text{kg/m}^2 \cdot \text{s}$ was given by the following equation:

$$N = 0.95 (X - 0.01)$$

where $X \rightarrow$ moisture content in kg moisture per kg of dry solid.

The slab is dried only from one side with the edges sealed. Density of the material is 1200 kg/m^3 . What is the time needed to reduce the moisture content from 35% to 5% on a wet basis?

- B3.** Potassium chloride (KCl) crystals of 1.1 mm average size are to be produced at a rate of 800 kg per batch in an evaporative crystallizer under vacuum at 40°C . At the start, the crystallizer is filled with a saturated solution of KCl and seeded with reasonably uniform-sized $80 \mu\text{m}$ crystals. A maximum slurry density of 150 kg of crystals per m^3 of slurry is allowed, and the crystal growth rate can be assumed to remain constant at $3 \times 10^{-8} \text{ m/s}$. Determine the following:

- (a) [8 points] Volume of crystallizer assuming the vessel was 70% filled at the beginning.
- (b) [8 points] Mass of seeds used.
- (c) [3 points] Batch time.
- (d) [6 points] Initial and final rate of evaporation.

DATA: Solubility of KCl in water at $40^\circ\text{C} = 400 \text{ kg/m}^3$
Density of KCl solution = 1300 kg/m^3
Density of crystals = 1900 kg/m^3
Shape factor of crystals = 1

