

**04-CHEM-A3, MASS TRANSFER OPERATIONS**

**DECEMBER 2016**

**Three Hours Duration**

**NOTES:**

- 1) If doubt exists as to the interpretation of any question, you are urged to submit a clear statement of any assumptions made along with the answer paper.
- 2) Property data required to solve a given problem are provided in the problem statement or are available in the recommended texts. If you are unable to locate the required data, do not let this prevent you from solving the rest of the problem. Even in the absence of property data, you still have the opportunity to provide a solution methodology.
- 3) This is an open-book exam.
- 4) Any non-communicating calculator is permitted.
- 5) The examination is in three parts – Part A (Questions 1 and 2)  
Part B (Questions 3 and 4)  
Part C (Questions 5 to 7)
- 6) Answer **ONE** question from Part A, **ONE** question from Part B, and **TWO** questions from Part C. **FOUR** questions constitute a complete paper.
- 7) Each question is of equal value.

PART A

- 1) A chamber of  $1 \text{ m}^3$  volume contains air at 293 K, 101.3 kPa and a partial pressure of water vapor of 0.8 kPa. A bowl of liquid with a free surface of  $0.01 \text{ m}^2$  and maintained at 303 K is introduced into the chamber. The mass transfer resistance is equivalent to that of a stagnant gas film of 0.25 mm thickness, and the effects of bulk flow can be neglected.

How long will it take for the air to become 90% saturated at 293 K? How much water must be evaporated?

DATA:            Saturation vapor pressure of water at 293 K = 2.3 kPa  
                      Saturation vapor pressure of water at 303 K = 4.3 kPa  
                      Diffusivity of water vapor in air =  $0.24 \text{ cm}^2/\text{s}$

- 2) Water evaporates at 350 K from an open bowl (30 cm diameter) into the atmosphere. The air currents are sufficiently strong to remove the water vapor as it is formed and the resistance to its mass transfer in air is equivalent to that of a 1 mm layer for conditions of molecular diffusion. The water can be considered as well mixed and the water equivalent of the system is equal to 10 kg.

What is the rate of cooling due to evaporation?

DATA:            Vapor pressure of water at 350 K =  $41.8 \text{ kN/m}^2$   
                      Diffusivity of water vapor in air =  $0.2 \text{ cm}^2/\text{s}$   
                      Specific volume of water vapor at NTP =  $22.4 \text{ m}^3/\text{kg}$   
                      Latent heat of vaporization of water at 350 K =  $2318 \text{ kJ/kg}$   
                      Specific heat capacity of water at 350 K =  $4.187 \text{ kJ/kg K}$

PART B

- 3) Ethanol at 289 K flows in a thin film down the outside surface of an inclined plane 2 meters wide and 4 meters long. Ethanol-free air at 303 K and 1 atm flows across the width of the plate parallel to the surface. At the average temperature of the gas film, the diffusivity of ethanol vapor in air is  $1.32 \times 10^{-5} \text{ m}^2/\text{s}$ . The vapor pressure of ethanol at 289 K is  $6.45 \times 10^{-2} \text{ atm}$ . The kinematic viscosity of ethanol vapor is  $1.533 \times 10^{-6} \text{ m}^2/\text{s}$ .

If the air velocity is 3 m/s, determine the rate at which liquid ethanol should be supplied to the top of the plate so that evaporation will prevent it from reaching the very bottom of the plate.

- 4) The absorption of carbon dioxide from carbon dioxide-air mixture in a solution containing  $100 \text{ kg/m}^3$  of sodium hydroxide were made in a 250 mm diameter tower packed to a height of 3 meters using 19 mm Raschig rings. The following results were obtained at atmospheric pressure;

$$\text{Gas rate} = 0.34 \text{ kg/m}^2\text{s}$$

$$\text{Liquid rate} = 3.94 \text{ kg/m}^2\text{s}$$

The carbon dioxide in the inlet gas was 315 parts per million and the carbon dioxide in the exit gas was 31 parts per million. Assume negligible vapor pressure of carbon dioxide over the solution.

What is the value of the overall gas mass transfer coefficient  $K_{Ga}$  in  $\text{kmol/s.m}^2\text{.(kPa)}$

**PART C**

- 5) A mixture of ethanol and water containing 16% mole of ethanol is continuously distilled in a plate-fractionating column to give a product containing 77% mole ethanol and a waste of 2% mole ethanol. It is proposed to withdraw 25% of ethanol in the entering stream as a side stream containing 50% mole of ethanol. The equilibrium mole fraction data for ethanol is given below:

<b><u>Liquid Mole Fraction</u></b>	<b><u>Vapor Mole Fraction</u></b>
0.00350	0.02050
0.00450	0.02750
0.01750	0.13150
0.05850	0.30500
0.06800	0.36150
0.09350	0.41100
0.16500	0.52000
0.21250	0.54550
0.24100	0.56750
0.36150	0.60600
0.47400	0.65050
0.49850	0.65550
0.58150	0.69700
0.64600	0.72900
0.72300	0.77600
0.79000	0.82000
0.83700	0.85200
0.87310	0.88170
0.88800	0.89300
0.89730	0.90120

Determine the number of theoretical plates required and the plate from which side the stream should be withdrawn if the feed is liquid at its boiling point and a reflux ratio of 2 is used.

- 6) Spherical particles (diameter = 15 nm, density = 2290 kg/m<sup>3</sup>) are pressed together to form a pellet. The following equilibrium data were obtained for the adsorption of nitrogen at 77 K:

<u>P/P<sup>0</sup></u>	<u>cm<sup>3</sup> liquid N<sub>2</sub>/kg solid</u>
0.1	66.7
0.2	75.2
0.3	83.9
0.4	93.4
0.5	108.4
0.6	130.0
0.7	150.2
0.8	202.0
0.9	348.0

Here P is the pressure of the adsorbate and P<sup>0</sup> is the vapor pressure of the adsorbate at 77K. The density of liquid nitrogen at 77 K is 808 kg/m<sup>3</sup>.

Obtain an estimate of the total surface area of the pellet from the adsorption isotherm.

- 7) 10 m<sup>3</sup> of a process fluid containing 20 kg/m<sup>3</sup> of an enzyme is to be concentrated to 200 kg/m<sup>3</sup> by means of ultrafiltration using membranes. Tests have shown that the enzyme is completely retained by a high-molecular weight, surface modified polysulfone membrane with a filtration flux (J, in m/hr) given by the following equation;

$$J = 0.04 \ln (250/C_f)$$

where C<sub>f</sub> is the enzyme concentration in kg/m<sup>3</sup>. Four hours is available for carrying out the process.

- (a) Calculate the area of membrane needed to carry out the concentration as a simple batch process.
- (b) The average filtration flux ( $J_{av}$ , in m/hr) during the simple batch process using the following approximation equation:

$$J_{av} = J_f + 0.27 (J_i - J_f)$$

where  $J_i$  is the initial filtration flux and  $J_f$  is the final filtration flux.

Is this approximation suitable for designing the membrane filtration process?

## The Periodic Table of the Elements

1																						18	
Hydrogen <b>1</b> H 1.01																						Helium <b>2</b> He 4.00	
Lithium <b>3</b> Li 6.94	Beryllium <b>4</b> Be 9.01																						
Sodium <b>11</b> Na 22.99	Magnesium <b>12</b> Mg 24.31																						
Potassium <b>19</b> K 39.10	Calcium <b>20</b> Ca 40.08																						
Rubidium <b>37</b> Rb 85.47	Strontium <b>38</b> Sr 87.62																						
Cesium <b>55</b> Cs 132.91	Barium <b>56</b> Ba 137.33	* 57-70																					
Francium <b>87</b> Fr (223)	Radium <b>88</b> Ra (226)	** 89-102																					
			3	4	5	6	7	8	9	10	11	12	13	14	15	16	17						
			Scandium <b>21</b> Sc 44.96	Titanium <b>22</b> Ti 47.88	Vanadium <b>23</b> V 50.94	Chromium <b>24</b> Cr 52.00	Manganese <b>25</b> Mn 54.94	Iron <b>26</b> Fe 55.85	Cobalt <b>27</b> Co 58.93	Nickel <b>28</b> Ni 58.69	Copper <b>29</b> Cu 63.55	Zinc <b>30</b> Zn 65.39	Gallium <b>31</b> Ga 69.72	Germanium <b>32</b> Ge 72.61	Arsenic <b>33</b> As 74.92	Selenium <b>34</b> Se 78.96	Bromine <b>35</b> Br 79.90	Krypton <b>36</b> Kr 83.80					
			Yttrium <b>39</b> Y 88.91	Zirconium <b>40</b> Zr 91.22	Niobium <b>41</b> Nb 92.91	Molybdenum <b>42</b> Mo 95.94	Technetium <b>43</b> Tc (98)	Ruthenium <b>44</b> Ru 101.07	Rhodium <b>45</b> Rh 102.91	Palladium <b>46</b> Pd 106.42	Silver <b>47</b> Ag 107.87	Cadmium <b>48</b> Cd 112.41	Indium <b>49</b> In 114.82	Tin <b>50</b> Sn 118.71	Antimony <b>51</b> Sb 121.76	Tellurium <b>52</b> Te 127.60	Iodine <b>53</b> I 126.90	Xenon <b>54</b> Xe 131.29					
			Lutetium <b>71</b> Lu 174.97	Hafnium <b>72</b> Hf 178.49	Tantalum <b>73</b> Ta 180.95	Tungsten <b>74</b> W 183.84	Rhenium <b>75</b> Re 186.21	Osmium <b>76</b> Os 190.23	Iridium <b>77</b> Ir 192.22	Platinum <b>78</b> Pt 195.08	Gold <b>79</b> Au 196.97	Mercury <b>80</b> Hg 200.59	Thallium <b>81</b> Tl 204.38	Lead <b>82</b> Pb 207.20	Bismuth <b>83</b> Bi 208.98	Polonium <b>84</b> Po (209)	Astatine <b>85</b> At (210)	Radon <b>86</b> Rn (222)					
			Lawrencium <b>103</b> Lr (262)	Rutherfordium <b>104</b> Rf (267)	Dubnium <b>105</b> Db (268)	Seaborgium <b>106</b> Sg (271)	Bohrium <b>107</b> Bh (272)	Hassium <b>108</b> Hs (270)	Meitnerium <b>109</b> Mt (276)	Darmstadtium <b>110</b> Ds (281)	Roentgenium <b>111</b> Rg (280)	Copernicium <b>112</b> Cn (285)	Ununtrium <b>113</b> Uut (284)	Ununquadium <b>114</b> Uuq (289)	Ununpentium <b>115</b> Uup (288)	Ununhexium <b>116</b> Uuh (293)	Ununseptium <b>117</b> Uus (294?)	Ununoctium <b>118</b> Uuo (294)					

- Alkali metals
- Alkaline earth metals
- Transition metals
- Other metals
- Metalloids (semi-metal)
- Nonmetals
- Halogens
- Noble gases

Element name → Mercury ← Atomic #

Symbol → Hg ← Avg. Mass

200.59

\*lanthanides

Lanthanum <b>57</b> La 138.91	Cerium <b>58</b> Ce 140.12	Praseodymium <b>59</b> Pr 140.91	Neodymium <b>60</b> Nd 144.24	Promethium <b>61</b> Pm (145)	Samarium <b>62</b> Sm 150.36	Europium <b>63</b> Eu 151.97	Gadolinium <b>64</b> Gd 157.25	Terbium <b>65</b> Tb 158.93	Dysprosium <b>66</b> Dy 162.50	Holmium <b>67</b> Ho 164.93	Erbium <b>68</b> Er 167.26	Thulium <b>69</b> Tm 168.93	Ytterbium <b>70</b> Yb 173.04
Actinium <b>89</b> Ac (227)	Thorium <b>90</b> Th 232.04	Protactinium <b>91</b> Pa 231.04	Uranium <b>92</b> U 238.03	Neptunium <b>93</b> Np (237)	Plutonium <b>94</b> Pu (244)	Americium <b>95</b> Am (243)	Curium <b>96</b> Cm (247)	Berkelium <b>97</b> Bk (247)	Californium <b>98</b> Cf (251)	Einsteinium <b>99</b> Es (252)	Fermium <b>100</b> Fm (257)	Mendelevium <b>101</b> Md (258)	Nobelium <b>102</b> No (259)

\*\*actinides

